

PVT Properties of Oil, Gas, and Water Add-in for Microsoft Excel

FOREWORD

The physical properties of petroleum fluids are required for most petroleum engineering calculations. During the 1980's an "application module" known as the Petroleum Fluids Pack was developed and marketed by Hewlett Packard for use in their HP-41 series programmable hand-held calculators. This software ROM utilized common empirical relationships to estimate PVT properties for oil, gas, and water. HP developed this set of programs with the assistance of Mr. D. N. Meehan (Champlin Petroleum Company) and Dr. H. J. Ramey (Stanford University). While the module and calculator that it required have not been available for many years, they remain popular with many petroleum engineers.

With the growth and adoption of desktop computers and spreadsheets for petroleum engineering calculations, a need to directly estimate PVT properties using spreadsheet functions similar to the original HP Petroleum Fluids Pack exists. This Microsoft Excel

4. From the Add-ins dialog box, click on browse and locate the PVTProps.XLA file that you saved in step 1.

Once installed, the fluid property functions can be accessed in any Excel formula in the same manner as other built-in numeric functions (i.e. sin, ln, etc.). The spreadsheet named "Example PVTProps.XLS" can be opened in Excel to view examples of the use of the functions. The basic code may also be inspected and modified if desired in the actual add-in file "PVTProps.XLA."

FUNCTION LIST

Bubble Point Pressure (psia)	BP(API, GOR, T, SG, SepT, SepP)
Critical Pressure for Miscellaneous Gases (psia)	Pcm(SG, N2, CO2, H2S)
Critical Temperature for Miscellaneous Gases (°R)	Tcm(SG, N2, CO2, H2S)
Gas Compressibility (psi ⁻¹)	Cg(P, T, SG, N2, CO2, H2S)
Gas Pressure from P/Z (psi) for Misc. Gases	Pressure(PoverZ, T, SG, N2, CO2, H2S)
Gas Pseudopressure (psi ² /centipoise)	mp(P, T, SG, N2, CO2, H2S)
Gas Viscosity (centipoise)	Ug(P, T, SG, N2, CO2, H2S)
Gas-Water Ratio (SCF/STBW)	3Tc 0 Tw 3.8 TD -0.0288 Tc 0. TCt.8 -13.833.833.833.833.8

BP(API, GOR, T, SG, SepT, SepP) Pcm(SG, N2, CO2, H2S) Tcm(SG, N2, CO2, H2S) Cg(P, T, SG, N2, CO2, H2S) Pressure(PoverZ, T, SG, N2, CO2, H2S) mp(P, T, SG, N2, CO2, H2S) Ug(P, T, SG, N2, CO2, H2S) 3Tc 0 Tw 3.8 TD -0.0288 Tc 0. TCt.8 -13.833.833.833.833.8
 0: Pcent ZZW Water Ratio SG, N2, Water CO2, H2S) Rate

FUNCTION DETAIL

Bubble Point Pressure (psia)

BP(API, GOR, T, SG, SepT, SepP)

Ranges of validity: $76 < \text{SepT} < 150^{\circ}\text{F}$
 $30 < \text{SepP} < 535 \text{ psia}$
For $15 < ^{\circ}\text{API} \leq 30$
 $0.511 < \text{SG} < 1.351$
For $30 < ^{\circ}\text{API} \leq 59.5$
 $0.530 < \text{SG} < 1.259$

Reference:

Vasquez, M., and Beggs, H. D., "Correlations for Fluid Physical Property Predictions," *Journal of Petroleum Technology*, June 1980, pp. 968-970.

Critical Pressure for Miscellaneous Gases (psia)

Pcm(SG, N2, CO2, H2S)

Critical Temperature for Miscellaneous Gases ($^{\circ}\text{R}$)

Tcm(SG, N2, CO2, H2S)

Ranges of validity: $0 \leq \% \text{N}_2 < 100$
 $0 \leq \% \text{CO}_2 < 100$
 $0 \leq \% \text{H}_2\text{S} < 100$
 $0 \leq \% \text{N}_2 + \% \text{CO}_2 + \% \text{H}_2\text{S} < 100$
 $0 \leq \% \text{CO}_2 + \% \text{H}_2\text{S} < 80$

Reference:

Standing, M. B., *Volumetric and Phase Behavior of Oil Field Hydrocarbon Systems*, 1977, pp. 26, 122.

Gas Compressibility (psi^{-1})

Cg(P, T, SG, N2, CO2, H2S)

Ranges of validity: same as Z factor.

References:

Meehan, D. N., and Lyons, W. K., "Calculations Programmable for TD (o Tw (able fo T

Gas Pseudopressure (psi²/centipoise)

mp(P, T, SG, N2, CO2, H2S)

Ranges of validity: same as Z factor and gas viscosity.

Note: This function uses the Z factor and gas viscosity correlations to numerically integrate the quantity $2P/\mu Z$ from a base of zero to the pressure P.

Gas Viscosity (centipoise)

Ug(P, T, SG, N2, CO2, H2S)

Ranges of validity: $40 < T < 460^{\circ}\text{F}$
 $14.7 < P < 10,000$ psi

References:

Lee, A. L., Gonzalez, M. H., and Eakin, B. E., "The Viscosity of Natural Gases," *Journal of Petroleum Technology*, August, 1966, pp. 997-1000.

Gonzalez, M. H., and Lee, A. L., "Graphical Viscosity Correlation for Hydrocarbons," *AIChE Journal*, March, 1968, pp. 242-244.

Gas-Water Ratio (SCF/STBW)

RSwat(T, P, Salt)

Ranges of validity: $90 < T < 250^{\circ}\text{F}$
 $500 < P < 5,000$ psia
 $0 \leq \text{Salt} < 3\%$ by weight

References:

Craft, B. C. and Hawkins, M. F., *Applied Petroleum Reservoir Engineering*, Prentice-Hall, 1959, p.130.

Ramey, H. J., Stanford University, unpublished correspondence.

Gas Z Factor

Z(P, T, SG, N2, CO2, H2S)

Ranges of validity: $1.05 < TR < 3.0$, where $TR \equiv T/T_{cm}$
 $0 < PR < 30$, where $PR \equiv P/P_{cm}$

Note: Other ranges of validity apply for the critical temperature and pressure that are estimated from the functions T_{cm} and P_{cm} listed below.

References:

Dranchuk, P. M., Purvis, R. A., and Robinson, D. B., "Computer Calculations of Natural Gas Compressibility Factors Using the Standing and Katz Correlation," *Institute of Petroleum Technical Series*, No. IP 74-008, 1974.

Takacs, G., "Comparisons Made for Computer Z-Factor Calculations," *Oil and Gas Journal*, Dec. 20, 1976, pp. 64-66.

Live Oil Viscosity (centipoise)

Uo(API, P, T, GOR, Pbp)

Below Bubble Point

For $15.3 < \text{°API} \leq 30$

$0.511 < \text{SG} < 1.351$

$14.7 < P < 4,542 \text{ psia}$

For $30 < \text{°API} \leq 59.5$

$0.530 < \text{SG} < 1.259$

$14.7 < P < 6,025 \text{ psia}$

References:

Ramey, H. J., "Rapid Methods of Estimating Reservoir Compressibilities," *Journal of Petroleum Technology*, April, 1964, pp. 447-454.

Vasquez, M., and Beggs, H. D., "Correlations for Fluid Physical Property Predictions," *Journal of Petroleum Technology*, June 1980, pp. 968-970.

Solution Gas-Oil Ratio (SCF/STBO)

RS(P, API, T, SG, SepT, SepP)

Ranges of validity: $76 < \text{SepT} < 150\text{°F}$

$30 < \text{SepP} < 535 \text{ psia}$

For $15 < \text{°API} \leq 30$

$0.511 < \text{SG} < 1.351$

$14.7 < P < 4,542 \text{ psia}$

For $30 < \text{°API} \leq 59.5$

$0.530 < \text{SG} < 1.259$

$14.7 < P < 6,025 \text{ psia}$

Reference:

Vasquez, M., and Beggs, H. D., "Correlations for Fluid Physical Property Predictions," *Journal of Petroleum Technology*, June 1980, pp. 968-970.

Water Compressibility (gas saturated) (psi⁻¹)

Cw(T, P, Rsw, Salt)

Ranges of validity: $80 < T < 250\text{°F}$

$1,000 < P < 6,000 \text{ psia}$

$0 \leq \text{Salt} < 25\% \text{ by weight}$

References:

Craft, B. C. and Hawkins, M. F., *Applied Petroleum Reservoir Engineering*, Prentice-Hall, 1959, p.130.

Meehan, D. N., "A Correlation for Water Compressibility," *Petroleum Engineer*, November, 1980, pp. 125-126.

Numere, D., Brigham, W. E., and Standing, M. B., *Correlations for Physical Properties of Petroleum Reservoir Brines*, Petroleum Research Institute, Stanford University, November, 1977, p. 17.

Water Formation Volume Factor (gas saturated) (rb/STBW)

Bw(T, P, Salt)

Ranges of validity: $100 < T < 250^{\circ}\text{F}$
 $1,000 < P < 5,000$ psia
 $0 \leq \text{Salt} < 25\%$ by weight

References:

Craft, B. C. and Hawkins, M. F., *Applied Petroleum Reservoir Engineering*, Prentice-Hall, 1959, p.131.

Numere, D., Brigham, W. E., and Standing, M. B., *Correlations for Physical Properties of Petroleum Reservoir Brines*, Petroleum Research